Stage1		
Vessel Pressure Drop	0.0000	kPa

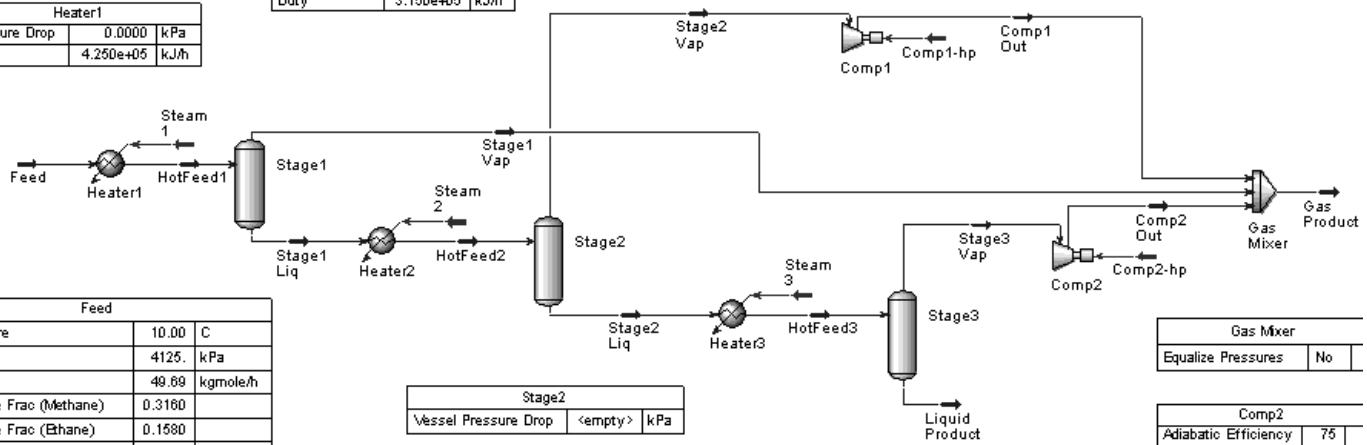
Heater1		
Pressure Drop	0.0000	kPa
Duty	4.250e+05	kJ/h

Heater2		
Pressure Drop	0.0000	kPa
Duty	3.150e+05	kJ/h

Stage2 Vap		
Pressure	2050.	kPa

Comp1		
Adiabatic Efficiency	75	

Comp1 Out		
Pressure	4125.	kPa



Feed		
Temperature	10.00	C
Pressure	4125.	kPa
Molar Flow	49.69	kgmole/h
Comp Mole Frac (Methane)	0.3160	
Comp Mole Frac (Ethane)	0.1580	
Comp Volume Frac (Propane)	0.1026	
Comp Mole Frac (i-Butane)	0.1050	
Comp Mole Frac (n-Butane)	0.1050	
Comp Mole Frac (i-Pentane)	0.0530	
Comp Mole Frac (n-Pentane)	0.0530	
Comp Mole Frac (n-Hexane)	0.0270	
Comp Mole Frac (n-Heptane)	0.0260	
Comp Mole Frac (n-Octane)	0.0260	
Comp Mole Frac (n-Nonane)	0.0260	

Stage2		
Vessel Pressure Drop	<empty>	kPa

Heater3		
Pressure Drop	0.0000	kPa
Duty	1.130e+05	kJ/h

Stage3		
Vessel Pressure Drop	<empty>	kPa

Stage3 Vap		
Pressure	350.0	kPa

Gas Mixer	
Equalize Pressures	No

Comp2		
Adiabatic Efficiency	75	

Comp2 Out		
Pressure	4125.	kPa